

GENESEE GENERATING STATION UNITS 4 AND 5 WATER CONSUMPTION AND EFFLUENT DISCHARGE CHARACTERIZATION REPORT

B&V PROJECT NO. 180144
B&V FILE NO. 41.0812 REV. 0

ISSUED FOR PERMIT APPLICATION

PREPARED FOR

Capital Power

19 SEPTEMBER 2013

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1.0 Objective

This data and information is being provided to support the Project Water Impact Assessment being conducted by Others for permitting purposes.

Based on the Project Block Diagram depicted on Drawing 180144-DN-0001 (Rev 0) and the water mass balance diagram 180144-WMB-1 (Rev 0), the major sources of project-related environmental water emissions are expected to include the following.

- Heat Recovery Steam Generator (HRSG) Blowdown
- Gas Turbine (GT) Air Inlet Evaporative Cooling Blowdown
- Project Drains through the Oil/Water Separator
- Water Treatment Wastewater
 - Filter backwash
 - Reverse osmosis reject
 - Mixed bed regenerant waste

1.1.1 Water Supply

Water supply for the Project is from the existing Genesee site cooling pond. The water mass balance and effluent discharge characterization were created using the cooling pond water quality data. (Attachment 1)

1.1.2 Water Effluent

Water effluent for the Project will be discharged to the Genesee site existing settling pond. The water flows and constituents indicated within this report are limited to the impact to the Genesee site from Genesee Generating Station Units 4 and 5.

2.0 Summary

The effluent discharge characterization is shown on the spreadsheet in Appendix A.

The Project water flow rates for the supply, use, evaporation, and effluent are depicted on the water mass balance diagram 180144-WMB-1 (Rev 0) in Appendix B.

3.0 Methodology and Analysis

The Project water flow rates for the supply, use, evaporation, and effluent are based upon the following:

1. HRSG Steam Cycle Makeup as 2% of Steam Turbine Flow with one third being lost as steam and two thirds being discharged as boiler blowdown.
2. GT Air Inlet Evaporative Cooling is based on Mitsubishi Power Systems data. Blowdown rate is based on 10 cycles of concentration in the evaporative cooler.
3. Project Drains through the Oil/Water Separator based on typical 2x1 Combined Cycle Power Plant B&V in-house data.
4. Filter backwash is based on backwashing the filters once per day.
5. Reverse osmosis reject is based on 75 percent recovery, traditional with fresh water sources.
6. The mixed bed regenerant waste is based on regenerating the resin once per week.
7. The boiler quench water flow is based on cooling the boiler blowdown to 140 °F.

Appendix A. Water Effluent Characterization Spreadsheet

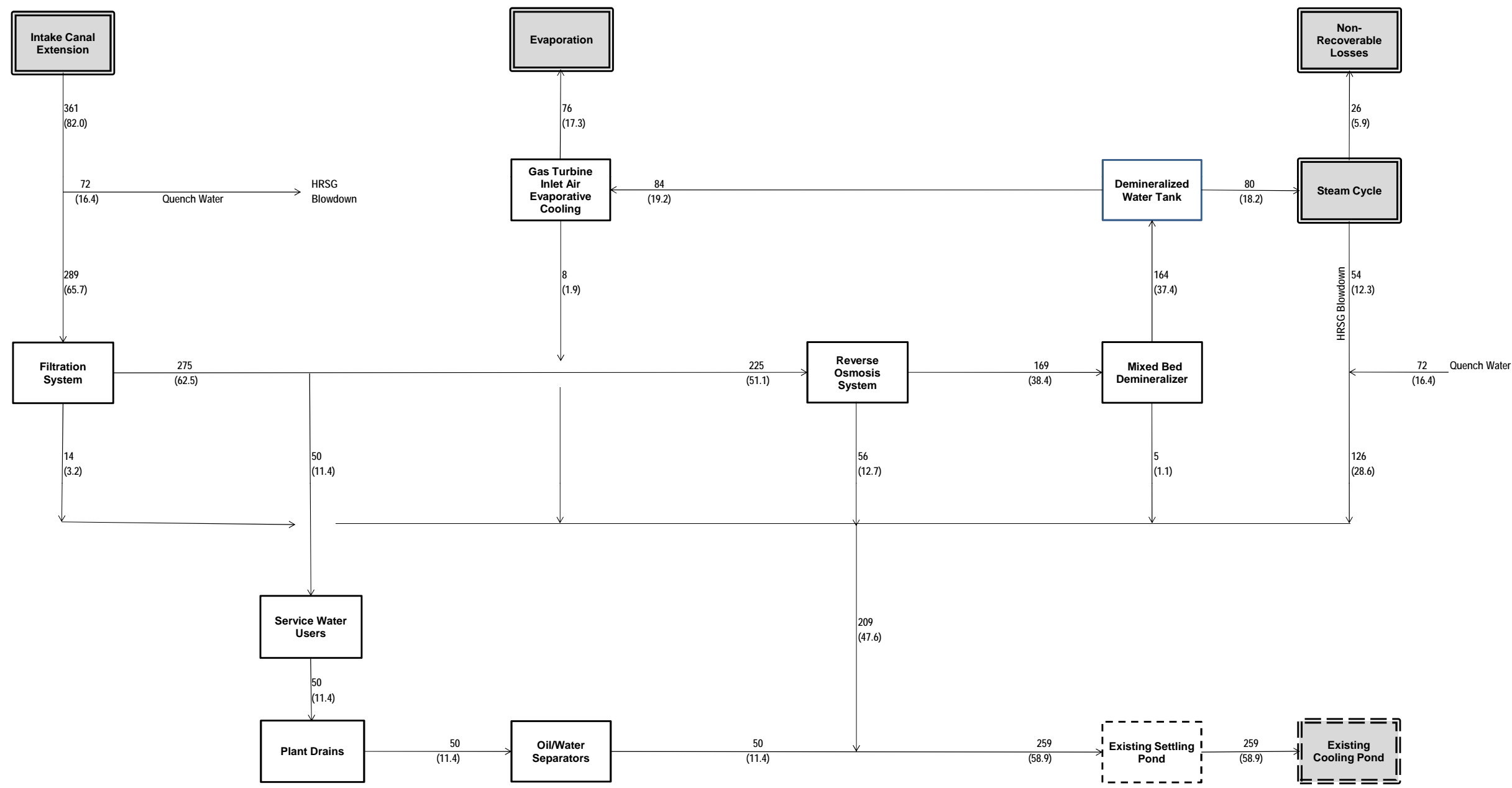
CAPITAL POWER
GENESEE GENERATING STATION UNITS 4 AND 5
PRELIMINARY WATER CONSUMPTION AND EFFLUENT DISCHARGE CHARACTERIZATION

	Raw Water	Filter Backwash	Service Water	RO Inlet	RO Effluent	RO Reject	MB Effluent	Mixed Bed Waste	HRSG Blowdown	Quenched Blowdown	Evap Cooler BD	Oil/water Separator	Effluent (Note 1)	
Flow (gpm)	289	14	275	225	169	56	164	5	54	126	8	50	255	Flow (gpm)
Ca (2.50 as CaCO3)	130	130	130	130	1.30	517	0	44	0	74	0	130	181	Ca (2.50 as CaCO3)
Mg (4.11 as CaCO3)	82	82	82	82	0.82	327	0	28	0	47	0	82	114	Mg (4.11 as CaCO3)
Na (2.17 as CaCO3)	74	74	74	74	0.74	293	0.003	6281	3	43	0	74	224	Na (2.17 as CaCO3)
K (1.28 as CaCO3)	6	6	6	6	0.06	25	0	2	0	4	0	6	9	K (1.28 as CaCO3)
Cations (as CaCO3)	292	292	292	292	2.92	1163	0	6355	3.0	168.4	0	292	527	Cations (as CaCO3)
M-Alk (as Ca CO₃)	260	260	260	260	2.60	1034	0	88	0	149	0	260	361	M-Alk (as Ca CO₃)
HCO3 (0.82 as CaCO3)	213	213.2	213.2	213	2.13	848	0	72	0	122	0	213	296	HCO3 (0.82 as CaCO3)
CO3 (1.67 as CaCO3)	0	0	0	0	0.00	0	0	0	0	0	0	0	0	CO3 (1.67 as CaCO3)
OH (2.94 as CaCO3)	0	0	0	0	0.00	0	0	0	0	0	0	0	0	OH (2.94 as CaCO3)
P (as CaCO3)	0	0.01	0.01	0	0.00	0	0	0	3	1	0	0	1	P (as CaCO3)
SO4 (1.04 as CaCO3)	82	82.16	82.16	82	0.82	327	0	6280	0	47	0	82	235	SO4 (1.04 as CaCO3)
Cl (1.41 as CaCO3)	8	8.46	8.46	8	0.08	34	0	3	0	5	0	8	12	Cl (1.41 as CaCO3)
NO3 (0.81 as CaCO3)	0.00	0	0	0	0.00	0	0	0	0	0	0	0	0	NO3 (0.81 as CaCO3)
CO2 (1.14 as CaCO3)	0.0	0	0	0	0.00	0	0	0	0	0	0	0	0	CO2 (1.14 as CaCO3)
SiO2 (0.83 as CaCO3)	37.5	37.5	37.5	38	0.38	149	0.01	13	0	21	0	38	52	SiO2 (0.83 as CaCO3)
Anions (as CaCO3)	304	304	304	304	3.04	1209	0	6355	3	175	0	304	543	Anions (as CaCO3)
pH	8.1	8.1	8.1	NA	NA	NA	NA	NA	NA	NA	NA	NA	8	pH
Cond., umhos/cm (calc)	532.0	532	532	532	10	2040	0.1	10000	10	308	0	513	910	Cond., umhos/cm (calc)
TDS (calculated), mg/L	345	345	345	345	5	1366	0	9064	3	287	0	501	724	TDS (calculated), mg/L
TSS, mg/L	100	2064	0	0	0	0	0	0	0	57	0	10	141	TSS, mg/L
Turbidity, NTU	0.00	0	0	0.00	0.00	0.00	0.00	0.00	1.00	57	25.00	10.00	30	Turbidity, NTU
Total hardness, mg/L	212.2	212.2	212.2	212.20	2.12	844.06	0	71.72	0	121	0.00	212.20	295	Total hardness, mg/L
Carbonate hardness, mg/L	212	212	212	212.00	2.12	843.27	0	71.66	0	121	0.00	212.00	295	Carbonate hardness, mg/L
Noncarbonate hardness, mg/L	0	0	0	0.00	0.00	0.00	0	0.00	0	0	0.00	0.00	0	Noncarbonate hardness, mg/L
Color, mg/L	15	15	15	15.00	0.15	59.67	0	5.07	0	9	0.00	15.00	21	Color, mg/L
Fe, mg/L	0.2	0.2	0.2	0.20	0.0020	0.80	0	0.07	0	0	0.00	0.20	0	Fe, mg/L
Mn, mg/L	0.1	0.1	0.1	0.10	0.0010	0.40	0	0.03	0	0	0.000	0.100	0	Mn, mg/L
Lead, mg/L	0.001	0.001	0.001	0.00	0.0000	0.00	0	0.00	0	0	0.000	0.0010	0	Lead, mg/L
Zn, mg/L	0.04	0.04	0.04	0.04	0.0004	0.16	0	0.01	0	0	0.00	0.04	0	Zn, mg/L
Hg, mg/L	0	0	0	0.00	0.0000	0.00	0	0.00	0	0	0.00	0.00	0	Hg, mg/L
Chromium, mg/L	0.003	0.003	0.003	0.00	0.0000	0.01	0	0.00	0	0	0.00	0.00	0	Chromium, mg/L
Cd, mg/L	0	0	0	0	0	0	0	0	0	0	0	0	0	Cd, mg/L
Arsenic, mg/L	0.007	0.007	0.007	0.007	0.00007	0.027844	0	0.002366	0	0.004	0	0.007	0	Arsenic, mg/L
Cu, mg/L	0.003	0.003	0.003	0.003	0.00003	0.011933	0	0.001014	0	0.001714	0	0.003	0	Cu, mg/L
Flouride (mg/L)	0.35	0.35	0.35	0.35	0.0035	1.392188	0	0.1183	0	0.2	0	0.35	0	Flouride (mg/L)
Ammonia Nitrogen (mg/L)	0.13	0.13	0.13	0.13	0.0013	0.517098	0	0.04394	0	0.074286	0	0.13	0	Ammonia Nitrogen (mg/L)
Temperature, Deg C														Temperature, Deg C

Note 1: Effluent does not include sanitary treatment effluent.

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Appendix B. Water Mass Balance



PRELIMINARY

NOTES	WATER BALANCE DESIGN INFORMATION				DRAWING INFORMATION				CAPITAL POWER	
1. ALL NON-PARENTHESIS FLOWS ARE IN GALLONS PER MINUTE - GPM.	FUEL	NATURAL GAS	CONDENSER COOLING	WET - ONCE THRU	ENG:	SAB	B&V PROJECT	180144	GENESEE GENERATING STATION	
2. ALL PARENTHESIS FLOWS ARE IN CUBIC METERS PER HOUR - CMH.	NET PLANT OUTPUT (MW)	TBD	COOLING POND CYCLES	N/A	DWG:	SAB	DRAWING NO.	WMB	UNITS 4 AND 5	
3. ALL FLOW RATES ARE PROJECT BASIS.	DRY BULB TEMP (C)	35.3	LOAD FACTOR	100%	CHK:	JRD	WMB CASE	1	PRELIMINARY WATER BALANCE	
4. THIS DRAWING IS PRELIMINARY AND SUBJECT TO FINAL MHI DESIGN DATA.	RELATIVE HUMIDITY	55%					REVISION	0	MHI 501J	
	DAY	MAX SUMMER					DATE	19-Sep-2013		
	HEAT BALANCE CASE	TBD					FILE	41.0812		

